

Catalysis Today 39 (1997) 33-44



Interaction between Mo and Co on Co–Mo/Al₂O₃ sulfided at high pressure (≤5.1 MPa) by means of high pressure DRIFT and EXAFS method

Naoto Koizumi, Masato Yamazaki, Shigeto Hatanaka, Muneyoshi Yamada*

Department of Applied Chemistry, Graduate School of Engineering, Tohoku University, Aoba, Aramaki, Aoba-ku, Sendai 980-77, Japan

Abstract

Co–Mo/Al₂O₃ was sulfided at high pressure (≤5.1 MPa) and was supplied for in-situ DRIFT measurement using NO as a surface probe molecule. The IR band of NO adsorbed on Co site was much stronger than that of Mo site, and the IR intensity ratio of Co site band to Mo site band was much higher when Co–Mo/Al₂O₃ was sulfided at the pressure above 1.1 MPa than when it was sulfided at atmospheric pressure. Mo/Al₂O₃, Co/Al₂O₃ and the physical mixture of them were also supplied for the high pressure DRIFT measurement. In the DRIFT spectra of the physical mixture, the intensity of the Mo site band was comparable to that of the Co site band. In the spectra of Ni–Mo/Al₂O₃, only the Ni site band was observed. Mo K-edge EXAFS showed that the dispersion of Mo of Co–Mo/Al₂O₃ is almost the same as that of the physical mixture and does not depend on the sulfiding pressure. Combining the results of the DRIFT spectra with that of Mo K-edge EXAFS, it was suggested that Co–Mo interaction induces selective formation of CUS on Co site on Co–Mo/Al₂O₃ and the interaction is promoted by higher pressure sulfiding. © 1997 Elsevier Science B.V.

Keywords: Co-Mo/Al₂O₃ catalyst; Ni-Mo/Al₂O₃ catalyst; High pressure sulfiding; Coordinatively unsaturated sites; DRIFT of adsorbed NO; Mo K-edge EXAFS

1. Introduction

Co-Mo/Al₂O₃ is widely used for the hydrotreatment of petroleum fractions. In order to meet the severe limitation for the environmental protection, every effort has been made to improve the conversion of HDS, HDN and HGN reactions on Co-Mo/Al₂O₃. For this purpose, the increase of the severity of the reaction conditions is necessary as well as the improvement of the catalyst performance. Not only

However, in the characterization of Co–Mo/Al₂O₃, the catalyst pretreating (sulfiding) conditions reported so far are limited to atmospheric pressure, which is far from the working state of Co–Mo/Al₂O₃. It is possible that the structure of Co–Mo/Al₂O₃ sulfided at atmospheric pressure is different from that of Co–Mo/Al₂O₃ sulfided at higher pressure.

Furthermore, the following points should be recalled. That is, the characterization techniques adopted so far are mainly Mössbauer and EXAFS,

to make clear the exact surface structure but also to improve catalyst performance further, it is necessary to observe the catalyst surface exposed to the severe reaction conditions.

^{*}Corresponding author. Tel.: (81-22) 217-7214; fax: (81-22) 217-7293.

whose information is predominated by the over-all structure of the catalyst, not by the surface structure.

In order to understand the surface structure of the catalyst at its working state, the present work tried to characterize the surface structure of Co–Mo/Al₂O₃ under its working state. That is, CUS distribution on the surface of Co–Mo/Al₂O₃ sulified at high pressure was investigated by DRIFT study of adsorbed NO using high temperature (≤773 K) and pressure (≤5.1 MPa) in-situ IR cell. Furthermore, fine structure around Mo of Co–Mo/Al₂O₃ was also investigated by Mo K-edge EXAFS using in-situ EXAFS cell. Our special attention was directed to the distribution of CUS on Co sites and Mo sites of Co–Mo/Al₂O₃.

2. Experimental

2.1. FT-IR/DRA of adsorbed NO

The catalyst, finely powdered, was placed in the high pressure DRIFT cell and 5% H₂S/H₂ was introduced into the cell at the pressure of 0.1-5.1 MPa, at room temperature. Under flowing 5% H₂S/H₂ (30 ml/min (STP)), the catalyst was heated to 673 K at the rate of 20 K/min. After the temperature reached 673 K, the temperature was held constant for 1 to 10 h. Then, the catalyst was cooled to room temperature, and He was introduced into the IR cell to purge 5% H₂S/H₂. Unless otherwise stated, sulfidation was carried out for 1 h.

10% NO/He was introduced to the IR cell by a pulse method. After flushing the gas-phase NO by He flow, FT-IR/DRA spectrum of NO adsorbed on the catalyst was measured by means of diffuse reflectance method using a FTS6000 (Bio-Rad) spectrometer equipped with mercury-cadmium-telluride detector.

2.2. Mo K-edge EXAFS

Finely powdered catalyst was pressed into pellets, which were set in the high pressure EXAFS cell. The EXAFS cell was designed and made according to that reported by Boudart et al. [1] 5% H₂S/H₂ was introduced into the EXAFS cell at the pressure of 0.1–5.1 MPa, at room temperature. Under flowing 5% H₂S/H₂ (150 ml/min (STP)), the catalyst was held at room temperature for 1 h, and then was heated to

673 K at the rate of 10 K/min. This temperature was kept for 2 h. After that, the catalyst was cooled to room temperature, and then He was introduced into the IR cell to flush 5% H₂S/H₂.

After these procedures, X-ray absorption spectra were measured using Laboratory System equipped with double-crystal monochromator [2,3]. The interatomic distances and the coordination numbers were determined by curve fitting techniques [4]. The back-scattering amplitudes and phase shifts reported by McKale et al. [5] were used. MoS₂ powder (supplied by Wako Pure Chemicals) was used as reference for Debye-Waller factor and photoelectron mean free path.

2.3. Catalyst preparation

Home-made Co-Mo/Al₂O₃, Mo/Al₂O₃ and Co/Al₂O₃ catalysts were used. Commercial Co-Mo/Al₂O₃ (supplied by Nippon Ketjen) was also used. In the following text, commercial Co-Mo/Al₂O₃ is denoted by Co-Mo/Al₂O₃ (NK) so as to distinguish it from home-made Co-Mo/Al₂O₃.

Home-made Co–Mo/Al₂O₃, Mo/Al₂O₃ and Co/Al₂O₃ were prepared by incipient wetness method. γ-Al₂O₃ (supplied by Nippon Ketjen, 333 m²/g, 0.76 cm³/g) was impregnated by (NH₄)₆Mo₇O₂₄·4H₂O (supplied by Wako Pure Chemicals) solution followed by drying (393 K, 16 h) and calcination (793 K, 12 h), then Mo/Al₂O₃ (MoO₃:15.8 wt%) was obtained. This was impregnated by Co(NO₃)₂·6H₂O (supplied by Wako Pure Chemicals) solution, followed by drying (393 K, 16 h) and calcination (793 K, 12 h); finally, Co–Mo/Al₂O₃ was obtained. Co/Mo molar ratio was fixed at that of Co–Mo/Al₂O₃ (NK) (0.56 mol/mol). Co/Al₂O₃ (CoO:5.2 wt%) was prepared as mentioned above.

3. Results and discussions

3.1. Effect of sulfiding pressure on the surface structure of Co-Mo/Al₂O₃

3.1.1. Distribution of CUS on Co-Mo/Al₂O₃, Mo/Al₂O₃ and Co/Al₂O₃

It is well known that NO adsorbs on CUS of Mo- or Co-Mo/Al₂O₃ catalyst. And it has been sometimes

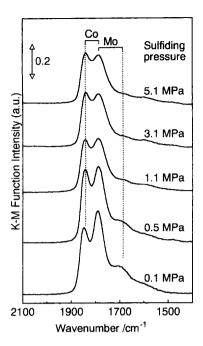


Fig. 1. DRIFT spectra of NO adsorbed on Co-Mo/Al₂O₃ sulfided at high pressure.

reported that the NO uptakes correlate well with the HDS activity. In the present work, in order to investigate the distribution of CUS on the catalyst surface, Co–Mo/Al₂O₃, Mo/Al₂O₃ and Co/Al₂O₃ sulfided at the pressure of 0.1–5.1 MPa were studied by means of high pressure DRIFT method using NO as a probe molecule.

Fig. 1 shows DRIFT spectra of NO adsorbed on Co-Mo/Al₂O₃ sulfided at the pressure of 0.1–5.1 MPa. Two bands appear in the spectrum on Co-Mo/Al₂O₃ at 1850 and 1800 cm⁻¹. A much weaker band also appears around 1700 cm⁻¹. From comparison with the spectra on Mo/Al₂O₃ and Co/Al₂O₃, the lower frequency (1800 and 1700 cm⁻¹) bands and higher frequency(1850 and 1800 cm⁻¹) bands can be assigned to NO adsorbed on Mo site-band and Co site-band, respectively. This assignment is consistent with that in our preceding papers using Co-Mo/Al₂O₃ sulfided at 0.1 MPa [6–8]. From here, we call the higher frequency bands the Co site-band, and the lower frequency bands the Mo site-band.

It is noticed that the spectrum of NO adsorbed on Co-Mo/Al₂O₃ sulfided above 1.1 MPa is different from that on Co-Mo/Al₂O₃ sulfided at 0.1 MPa. That is, increasing the sulfiding pressure above 1.1 MPa,

only two bands appear, and the lower frequency Mo site-band seems to disappear. Clearly, the intensity ratio of Co site-band to Mo site-band is much higher when Co–Mo/Al₂O₃ is sulfided over 1.1 MPa than when it is sulfided at 0.1 MPa. It is also noticed that no drastic change appears with increasing sulfiding pressure above 1.1 MPa.

These spectra show that the CUS is selectively formed on Co site of Co-Mo/Al₂O₃ sulfided at every pressure, especially above 1.1 MPa.

Fig. 2(a,b) show the FT-IR/DRA spectra of NO adsorbed on Mo/Al₂O₃ and Co/Al₂O₃, respectively, which are sulfided at 0.1–5.1 MPa. The spectra on Mo-and Co/Al₂O₃ show two bands, respectively. This doublet has been well known and has been assigned to dinitrosyl species adsorbed on Mo site or Co site. Increasing the sulfiding pressure, the shape of the doublet gradually changes. That is, the lower frequency band relatively increases.

Comparing Fig. 1 with Fig. 2(a,b), it is clear that the spectrum of NO adsorbed on Co–Mo/Al₂O₃ is not a simple superposition of those on Mo/Al₂O₃ and Co/Al₂O₃. That is, the IR intensity of Mo site-band in Co–Mo/Al₂O₃ is very weak. However, it is not sure whether the CUS is selectively formed on Co sites, or the CUS on Mo sites selectively disappears.

3.1.2. Intrinsic effect of sulfiding pressure and the stability of surface structure

As mentioned above, the sulfiding pressure clearly affects the distribution of CUS on Co–Mo/Al₂O₃. Therefore, the sulfiding pressure may be an important factor influencing the surface structure of the catalyst. In order to confirm this possibility, the effect of the sulfiding pressure was further studied from a different point of view; that is, the effect of sulfiding duration and the stability of the surface structure at its working state.

Concerning the former, FT-IR/DRA spectra of NO adsorbed on Co-Mo/Al₂O₃ sulfided at 0.1 MPa for the time of 1-10 h are shown in Fig. 3. The relative intensity of Co site-band slightly increases with increasing sulfiding time. However, comparing Fig. 1 with Fig. 3, the relative intensity of Co site-band of Co-Mo/Al₂O₃ sulfided at 1.1 MPa (for 1 h) is stronger than that of Co-Mo/Al₂O₃ sulfided at 0.1 MPa for 10 h. These results indicate that the surface structural change induced by 1.1 MPa sulfiding

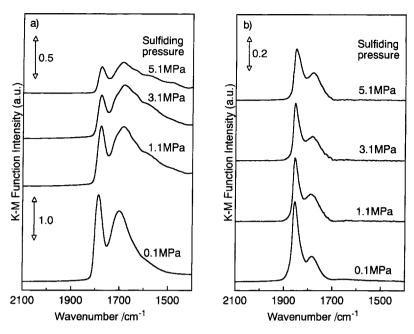


Fig. 2. DRIFT spectra of NO adsorbed on the catalysts sulfided at high pressure. (a) Mo/Al₂O₃ and (b) Co/Al₂O₃.

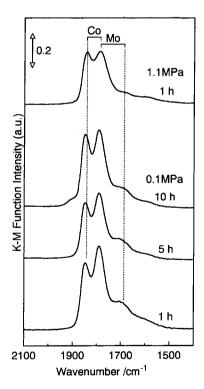


Fig. 3. Comparison of the spectrum on $Co-Mo/Al_2O_3$ sulfided at 1.1 MPa with those on $Co-Mo/Al_2O_3$ sulfided at 0.1 MPa with various sulfiding durations.

can not be attained by simple extension of sulfiding duration at 0.1 MPa.

Concerning the latter, it should be recalled that the catalyst in industrial HDS process is usually exposed to a high pressure hydrogen stream under its working state after presulfiding. It is possible that the surface structure of the catalyst, once sulfided, is changed by this exposing to a hydrogen stream. Here, the CUS of the catalyst which was reduced in the stream of hydrogen after the presulfiding was examined by the same DRIFT method using NO as a probe molecule. Fig. 4 shows the DRIFT spectra of NO adsorbed on Co-Mo/Al₂O₃, which was sulfided in 5% H₂S/H₂ stream and then reduced in the stream of H₂ at 673 K under 3.1 MPa. The spectra of adsorbed NO is almost the same as that of the catalyst just sulfided. Even after 10 h of reducing, the spectra is little changed. For comparison, in Fig. 4 are also shown the spectra of the catalyst which was reduced initially in the stream H₂ and then sulfided in the stream of H₂S/H₂ stream. The surface structure of the catalyst reduced initially and then sulfided is different from that of the catalyst sulfided initially and then reduced. It can be said that the catalyst surface is sensitive to the pretreatment, especially presulfiding or prereducing. These spectra suggest that the surface structure of Co-Mo/Al₂O₃

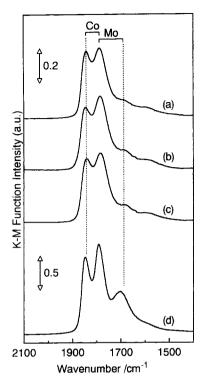


Fig. 4. Comparison of the spectrum on $Co-Mo/Al_2O_3$ sulfided at 1.1 MPa with those on variously pretreated $Co-Mo/Al_2O_3$. (a) Sulfided at 1.1 MPa, (b) sulfided at 1.1 MPa then reduced at 3.1 MPa for 2 h, (c) sulfided at 1.1 MPa then reduced at 3.1 MPa for 10 h and (d) reduced at 1.1 MPa then sulfided at 1.1 MPa.

once presulfided is stable under high pressure of hydrogen.

3.1.3. Effect of loading amount on the interaction between Mo and Co on the support

What kind of interaction is working between Mo and Co on the support? And how the interaction is changed with increasing the sulfiding pressure.

The interaction between Co and Mo on the support may be affected by the loading amount of Co and Mo. It is possible that higher loading promotes the interaction between Co and Mo.

We prepared the catalyst with half loading, and studied the DRIFT spectra of NO adsorbed on them and studied the effect of loading amount on the interaction between Co and Mo. The results are shown in Fig. 5. As we can see, the DRIFT spectra shows the same pressure dependency as the full loading catalyst. That is, the Mo site-band is very

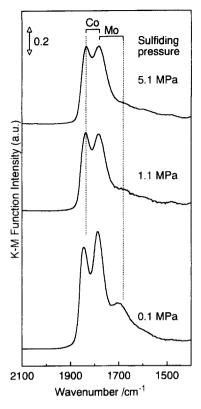


Fig. 5. DRIFT spectra of NO adsorbed on Co-Mo/Al₂O₃ (MoO₃:7.7 wt%,Co/Mo:0.56 mol/mol) sulfided at 0.1, 1.1 and 5.1 MPa.

weak at high pressure sulfiding. The results suggest that CUS is selectively formed on Co sites even on the half loading catalyst.

3.2. Interaction between Mo and Co on the support

3.2.1. Distribution of CUS on a physical mixture of Mo/Al_2O_3 and Co/Al_2O_3

As mentioned above, the characteristic distribution of CUS observed on Co-Mo/Al₂O₃ sulfided at high pressure is widely observed in other cases, i.e. long time-sulfided catalyst, sulfided then reduced catalyst, and low loading catalyst.

To understand the surface structure of Co–Mo/Al₂O₃ sulfided at high pressure in more detail, we studied the sulfiding pressure dependency of the physical mixture of Mo/Al₂O₃ and Co/Al₂O₃. A physical mixture of Mo/Al₂O₃ and Co/Al₂O₃ was supplied for DRIFT study of adsorbed NO. Co/Mo molar ratio of

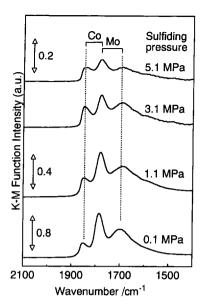


Fig. 6. DRIFT spectra of NO adsorbed on a physical mixture of Mo/Al_2O_3 and Co/Al_2O_3 .

the physical mixture was fixed at 0.56, which is equal to that of Co-Mo/Al₂O₃. Fig. 6 shows the obtained spectra of NO adsorbed on the physical mixture sulfided at the pressure of 0.1-5.1 MPa. Three bands appear in the range of NO stretching vibration at every pressure of sulfiding. These bands can be assigned to Co and Mo site-band respectively, referring to the spectra of Mo/Al₂O₃ (Fig. 2(a)) and Co/Al₂O₃ (Fig. 2(b)). The intensity of Mo site-band is comparable to that of Co site-band, and does not disappear with increasing sulfiding pressure. In other words, the distribution of CUS of the physical mixture is not affected by sulfiding pressure. Comparing Fig. 6 with Fig. 2(a,b), it is clear that the spectra of NO adsorbed on the physical mixture seems to be a simple superposition of those on Mo/Al₂O₃ and Co/Al₂O₃. This will be discussed in Section 3.2.3.

Here, we will compare the spectra of the physical mixture with that of Co–Mo/Al₂O₃. It is easy to point out the difference between them. As we can see, three bands appear in the spectrum of physical mixture. On the other hand, two bands appear in the spectrum of Co–Mo/Al₂O₃. The distribution of CUS is clearly different between Co–Mo/Al₂O₃ and the physical mixture of Mo- and Co/Al₂O₃. Furthermore, it is noted that the difference became more profound with increasing the sulfiding pressure.

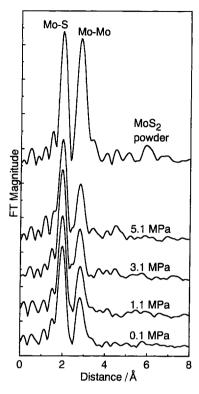


Fig. 7. Fourier transforms of Mo K-edge EXAFS of Co–Mo/Al $_2$ O $_3$ sulfided at high pressure.

3.2.2. Effect of sulfiding pressure on the morphology of MoS₂-like structure

As mentioned above, the present results showed that Mo site of Co–Mo/Al₂O₃ has a lower number of CUS compared to Mo/Al₂O₃ and the higher pressure of sulfiding decreases the relative ratio of CUS on Mo sites. These two points were investigated from the point of the dispersion of Mo. Because it is possible that the decrease of CUS on Mo site correlates with the morphology of a MoS₂-like structure, that is, the growth of MoS₂-like structure in the lateral direction. Therefore, the change of the dispersion of Mo site accompanied by high pressure sulfiding was examined by means of the Mo K-edge EXAFS method.

Fig. 7 shows the Fourier transforms of Mo K-edge EXAFS spectra (radial structure function) of Co-Mo/Al₂O₃ sulfided at the pressure of 0.1-5.1 MPa. Fig. 7 also shows that of MoS₂ powder for reference. As shown in Fig. 7, only Mo-S and Mo-Mo shells clearly appear in the radial structure function of the catalysts sulfided at the pressure of 0.1-5.1 MPa. These two

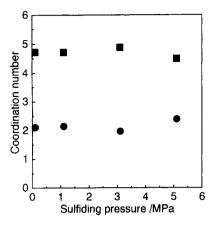


Fig. 8. Dependency of the coordination number of Mo–S shell (■) and Mo–Mo shell (●) on the sulfiding pressure (Co–Mo/Al₂O₃).

peaks suggest that the fine structure around Mo in Co-Mo/Al₂O₃ can be approximated by MoS₂-like structure when Co-Mo/Al₂O₃ is sulfided at the pressure of 0.1-5.1 MPa. It is noticed that the peak intensities of Mo-S and Mo-Mo shells are hardly affected by sulfiding pressure. Coordination numbers calculated about Mo-S and Mo-Mo shells of Co-Mo/Al₂O₃ are shown in Fig. 8. As can be seen from Fig. 8, both Mo-S and Mo-Mo coordination numbers are almost constant in the range of 0.1-5.1 MPa. These results suggest that the morphology of MoS₂-like structure formed in Co-Mo/Al₂O₃ is hardly affected by higher pressure sulfiding.

Fig. 9 shows the radial structure function of the physical mixture sulfided at 0.1, 1.1 and 5.1 MPa. The physical mixture examined here is the same as that for the FT-IR/DRA measurement already mentioned. Mo-S and Mo-Mo coordination numbers of the physical mixture are shown in Fig. 10. Comparing Co-Mo/Al₂O₃ with the physical mixture, Mo-Mo coordination number of Co-Mo/Al₂O₃ is constant, and comparable with that of the physical mixture in the range of 0.1-5.1 MPa. This suggests that the growth of MoS₂-like structure in the lateral direction on Co-Mo/Al₂O₃ is comparable with that on the physical mixture. It can be said that the presence of Co does not affect the morphology of MoS₂-like structure of sulfided Co-Mo/Al₂O₃.

The present Mo K-edge EXAFS studies show that the morphology of MoS₂-like structure of Co–Mo/ Al₂O₃ is hardly affected by high pressure sulfiding and

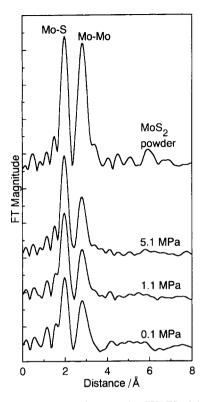


Fig. 9. Fourier transforms of Mo K-edge EXAFS of the physical mixture of Mo/Al₂O₃ and Co/Al₂O₃ sulfided at 0.1, 1.1 and 5.1 MPa.

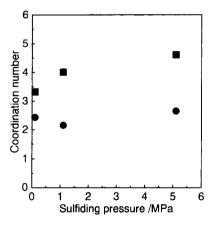


Fig. 10. Dependency of the coordination number of Mo–S shell (■) and Mo–Mo shell (●) on the sulfiding pressure (the physical mixture of Mo/Al₂O₃ and Co/Al₂O₃).

the presence of Co. Therefore, it can be said that the surface structural change induced on Co–Mo/Al₂O₃ by high pressure sulfiding is not accompanied by the growth of MoS₂-like structure in the lateral direction.

However, the reason why Mo has no CUS on Co-Mo/Al₂O₃ is still unclear. What is the reason of the selective disappearance of CUS on Mo site, or the selective formation of CUS on Co site on Co-Mo/Al₂O₃? Furthermore, what is the reason why the higher pressure of sulfiding increases the selectivity of the disappearance of CUS on Mo site?

The change accompanied by high pressure sulfiding may be due to an interaction between Mo and Co on the support. What kind of interaction is working between Mo and Co on the support?

3.2.3. Curve fitting analyses of the spectra of the catalysts by linear combination of the spectra of components

As mentioned above, Mo K-edge EXAFS shows that the dispersion of Mo does not change within this range of sulfiding pressure. Here, in order to investigate the reason why Mo site of Co-Mo/Al₂O₃ has no CUS after high pressure sulfiding, the spectra of Co-Mo/Al₂O₃ were compared with those of Co/Al₂O₃ and Mo/Al₂O₃, and the differences between them were analyzed by a curve fitting method.

Now, we tried to analyze these bands by a linear combination of the IR band of each component (i.e. Mo/Al₂O₃ and Co/Al₂O₃). First of all, in order to obtain the weight of Co site-band, the IR band intensity of Co/Al₂O₃ is adjusted to that of the highest frequency band. Second, the weight of Mo site-band is obtained by adjusting the band intensity of Mo/Al₂O₃ to the lowest frequency band. Then, the spectrum of each component is combined together, depending on each weight. By doing this, we can obtain a good fitting of a linear combination of Mo/Al₂O₃ and Co/Al₂O₃ to that of the physical mixture, as shown in Fig. 11. It can be said that the IR band of the physical mixture is well explained by a linear combination of Mo/Al₂O₃ and Co/Al₂O₃. This result is reasonable because Co and Mo in the physical mixture do not interact.

Then we tried to analyze the IR band of Co–Mo/Al₂O₃ in the same manner as mentioned above. As shown in Fig. 12, the fitting between the IR band of Co–Mo/Al₂O₃ and that of the linear combination of Mo/Al₂O₃ and Co/Al₂O₃ is not good. That is, the spectrum on Co–Mo/Al₂O₃ can not be expressed by the linear combination of those on Mo and Co/Al₂O₃.

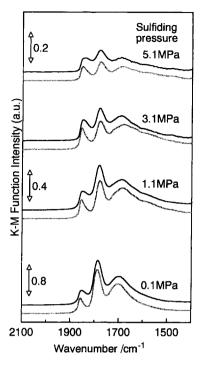


Fig. 11. Curve fitting analysis of the spectra on the physical mixture of Mo/Al_2O_3 and Co/Al_2O_3 . The spectra on the physical mixture of Mo/Al_2O_3 and Co/Al_2O_3 (continuous line) and the linear combination of the spectra on Mo/Al_2O_3 and Co/Al_2O_3 (dashed line).

It is further noted that the discrepancy increases with increasing the sulfiding pressure.

The curve fitting method showed that the distribution of CUS on $\text{Co-Mo/Al}_2\text{O}_3$ is different from that of the physical mixture and can not be expressed by a linear combination of the spectra of each component. Especially it is noted that the CUS of $\text{Mo/Al}_2\text{O}_3$ drastically disappears when Mo exists with Co on the support.

3.3. Effect of sulfiding pressure on the surface structure of Ni–Mo/Al₂O₃

For comparison, Ni-Mo/Al₂O₃ was also supplied for DRIFT measurement. Fig. 13 shows FT-IR/DRA spectra of NO adsorbed on Ni-Mo/Al₂O₃ sulfided at the pressure of 0.1-5.1 MPa. An asymmetric absorption band appears at 1840 cm⁻¹ in every pressure of sulfiding. Much weaker and broader band appears around 1700 cm⁻¹ in both cases. The spectra of NO

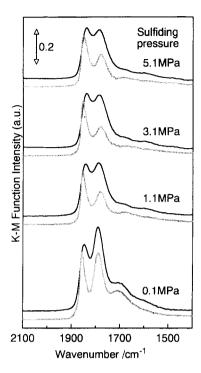


Fig. 12. Curve fitting analysis of the spectra on $Co-Mo/Al_2O_3$. The spectra on $Co-Mo/Al_2O_3$ (continuous line) and the linear combination of the spectra on Mo/Al_2O_3 and Co/Al_2O_3 (dashed line).

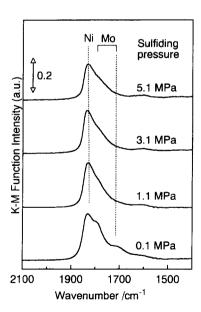


Fig. 13. DRIFT spectra of NO adsorbed on $Ni-Mo/Al_2O_3$ sulfided at high pressure.

adsorbed on Mo/Al₂O₃ and Ni/Al₂O₃ are also shown in Fig. 14(a,b). Based on the spectra of the reference samples, the asymmetric band in Ni–Mo/Al₂O₃ can be assigned to NO adsorbed on Ni site. The IR intensity of the Ni site-band is insensitive to the change of the sulfiding pressure. On the other hand, two weak bands assigned to NO adsorbed on Mo site appear in the catalyst sulfided at 0.1 MPa but diminish after sulfiding above 1.1 MPa.

The DRIFT spectra of NO adsorbed on Ni-Mo/Al₂O₃ is basically similar to that of Co-Mo/Al₂O₃. That is, CUS is selectively formed on the promoter sites, even at lower pressure of sulfiding.

In the spectra of Ni/Al₂O₃, an asymmetric band appears. This band can be assigned to the dinitrosyl species adsorbed on Ni site. The reason why the band looks like a singlet is due to the molecular structure of dinitrosyl species.

In Fig. 15 are also shown the spectra of a physical mixture of Mo/Al₂O₃ and Ni/Al₂O₃. Ni/Mo molar ratio of the physical mixture was 0.56, which is equal to that of Ni–Mo/Al₂O₃. Both the Ni site-band and Mo site-band clearly appear in every pressure.

Comparing the spectra of Ni-Mo/Al₂O₃ with that of the physical mixture, it is noted that the intensity of Mo-site band of Ni-Mo/Al₂O₃ is much weaker than that of the physical mixture in every pressure of sulfiding. This suggests that Ni interacts with Mo as well as Co.

The DRIFT spectra of Ni-Mo/Al₂O₃ and the physical mixture of Mo/Al₂O₃ and Ni/Al₂O₃ were also analyzed in the same manner. The spectra of the physical mixture can be well expressed by a linear combination of the spectrum of Mo/Al₂O₃ and Ni/Al₂O₃. Ni-Mo/Al₂O₃ is also well expressed by the linear combination, in which the weight of the spectrum of Mo/Al₂O₃ is negligible. It can be said that CUS of Ni-Mo/Al₂O₃ is very selectively formed on Ni site at every pressure of sulfiding.

3.4. Surface structure of Co-Mo/Al₂O₃ formed by high pressure sulfiding

The recent developments of surface analysis techniques contribute to evaluating the surface structure of Co-Mo/Al₂O₃; some models of active sites for HDS reaction are proposed. That is, Topsøe et al. have proposed 'Co-Mo-S' model by means of Mössbauer

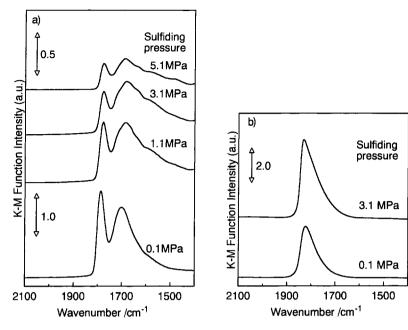


Fig. 14. DRIFT spectra of NO adsorbed on the catalysts sulfided at high pressure. (a) Mo/Al₂O₃ and (b) Ni/Al₂O₃.

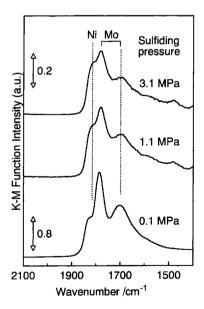


Fig. 15. DRIFT spectra of NO adsorbed on a physical mixture of Mo/Al₂O₃ and Ni/Al₂O₃ sulfided at 0.1, 1.1 and 3.1 MPa.

emission spectroscopy (MES) as the active site for HDS of thiophenes on Co–Mo/Al₂O₃ [9,10]. Furthermore, local structure of 'Co–Mo–S' on Co–Mo/active-C has been proposed by means of Mo and Co K-edge EXAFS [11,12].

However, some problems about 'Co-Mo-S' model are pointed out. One is that there is a complexity with signal assignment in MES. That is, it has been reported that 'Co-Mo-S' like Mössbauer signal appears even in Co/active-C [13]. This might make ambiguous the fact that the intensity of 'Co-Mo-S' signal in MES correlates with thiophene HDS activity. The other is concerning the stability of 'Co-Mo-S' in reaction conditions. That is, Breysse et al. have reported the results of MES and XPS of unsupported Co-Mo sulfides using HDS of dibenzothiophene under pressurized conditions [14,15,16]. Based on these results, they speculated that Co in 'Co-Mo-S' on unsupported Co-Mo sulfide was segregated in their reaction condition. This speculation does not necessarily exclude the existence of 'Co-Mo-S' on Co-Mo/Al₂O₃, but might limit the role of 'Co-Mo-S' in industrial HDS reaction. Also in relation to this problem, a 'Remote control model' has been proposed by Delmon et al. [17]

These problems indicate the need to recall some points should be reminded about experimental techniques. That is, (i) the characterization techniques adopted so far are mainly MES and EXAFS, whose information is predominated by the over-all structure of the catalysts, not by the surface structure. There-

combining these with surface sensitive techniques is necessary to evaluate the surface structure of Co-Mo/Al₂O₃ more clearly. And (ii) the catalyst pretreating (sulfiding) conditions reported so far are limited to atmospheric pressure, which is far from the working state of Co-Mo/Al₂O₃. It is possible that the surface structure of Co-Mo/ Al₂O₃ sulfided at atmospheric pressure is different from that of Co-Mo/Al₂O₃ sulfided at higher pressure. In order to clarify the active sites for industrial HDS reaction on Co-Mo/Al₂O₃, it is necessary to characterize the surface structure of Co-Mo/ Al₂O₃ under its working state, at least to evaluate insitu (without exposing the catalyst to the air) the surface structure of Co-Mo/Al₂O₃ sulfided at high pressure.

In relation to problem (i), the authors have characterized the surface structure of Co-Mo/Al₂O₃ by combining NO probe method (NO uptake measurement and FT-IR/DRA study of adsorbed NO) as surface sensitive technique and Mo K-edge EXAFS. and found the new aspects of active site on Co-Mo/ Al₂O₃. That is, we have investigated the benzothiophene HDS activity and the surface structure of Co-Mo/Al₂O₃ which is pretreated by combination of sulfiding and reducing, and reported that the formation ratio of Co site to Mo site correlates with the benzothiophene HDS efficiency [6]. In addition, comparing the surface structure of Co-Mo/Al₂O₃ with that of Ni-Mo/Al₂O₃ and Fe-Mo/Al₂O₃ in detail, it was found that the growth of MoS₂-like structure in the lateral direction on Fe-Mo/Al₂O₃, in which synergy effects for HDS of benzothiophene do not appear, is suppressed compared to that on Co-Mo/Al₂O₃ and Ni-Mo/Al₂O₃ [18,19]. However, in these studies, problem (ii) remains unsolved.

In the present work, we tried to study the surface structure of Co–Mo/Al₂O₃ under its working state by high pressure DRIFT method. That is, CUS distribution on the surface of Co–Mo/Al₂O₃ sulfided at high pressure was investigated by FT–IR/DRA study of adsorbed NO using high temperature (≤773 K) and pressure (≤5.1 MPa) in-situ IR cell. Furthermore, the fine structure around Mo of Co–Mo/Al₂O₃ was also investigated by Mo K-edge EXAFS using in-situ EXAFS cell.

As the results, we have found that the sulfiding pressure clearly changes the surface structure. Com-

paring Co-Mo/Al₂O₃ with the physical mixture, the following two points are noted. (A) The relative intensity of Co site-band of Co-Mo/Al₂O₃ is much stronger than that of the physical mixture in the range of 0.1-5.1 MPa. This suggests that Co site is selectively formed on Co-Mo/Al₂O₃, compared to the physical mixture of Mo/Al₂O₃ and Co/Al₂O₃. (B) it is also noted that the difference of the relative intensity of Co site-band between them is remarkable when the catalysts are sulfided at the pressure above 1.1 MPa. This suggests that Co site is more profoundly formed when Co-Mo/Al₂O₃ is sulfided at the pressure above 1.1 MPa. These two phenomena (A) and (B) suggest that a kind of surface interaction species is effectively formed between Co and Mo when Co-Mo/Al₂O₂ is sulfided at high pressure.

4. Conclusion

In order to evaluate the surface structure of Co-Mo/ Al₂O₃ under its working state, the distributions of CUS of Co-Mo/Al₂O₃ and the physical mixture of Mo/Al₂O₃ and Co/Al₂O₃ sulfided at high pressure (≤5.1 MPa) were investigated in-situ by FT-IR/ DRA study of adsorbed NO. It was found that the CUS was selectively formed on Co site of Co-Mo/ Al₂O₃, and the selectivity was clearly increased by higher pressure of sulfiding. On the other hand, Mo K-edge EXAFS measurement indicated that the dispersion of Mo does not change by higher pressure of sulfiding. Therefore, the selective formation of CUS on Co site is not due to the selective sintering of Mo site of Co-Mo/Al₂O₃. Based on these results, it was suggested that Co-Mo interaction species is effectively formed by higher pressure sulfiding. The present work shows more straightforward results, based on which one can discuss about the surface structure of Co-Mo/Al₂O₃ under its working state with respect to Co and Mo site distribution.

Acknowledgements

We thank Professor Yasuo Udagawa for useful discussions concerned with EXAFS measurements and for the use of the EXAFS spectrometer. This work was supported by a Grant-in-Aid for Scientific

Research from the Ministry of Education, Science, Sports and Culture of Japan.

References

- R.A. Dalla Betta, M. Boudart, K. Foger, D.G. Löffler, Sanchez-Arrieta, Rev. Sci. Instrum. 55 (1984) 1910.
- [2] K. Tohji, Y. Udagawa, T. Kawasaki, K. Mieno, Rev. Sci. Instrum. 59 (1988) 1127.
- [3] Y. Udagawa, Rigaku J. 6 (1989) 20.
- [4] K. Tohji, Y. Udagawa, S. Tanabe, A. Ueno, J. Am. Chem. Soc. 106 (1984) 612.
- [5] A.G. McKale, B.W. Veal, A.P. Paulikas, S.-K. Chan, G.S. Knapp, J. Am. Chem. Soc. 110 (1988) 3763.
- [6] S. Kasahara, S. Miyabe, T. Shimizu, H. Takase, M. Yamada, Sekiyu Gakkaishi 38 (1995) 81.
- [7] T. Obara, M. Yamada, A. Amano, Chem. Lett. 1986, 2003.
- [8] M. Yamada, S. Kasahara, K. Kawahara, in: T. Inui, K. Fujimoto, T. Uchijima, M. Masai (Eds.), New Aspects of

- Spillover Effect in Catalysis, Elsevier, Amsterdam, 1993, p. 349.
- [9] N.-Y. Topsøe, H. Topsøe, J. Catal. 84 (1983) 386.
- [10] H. Topsøe, B.S. Clausen, Catal. Rev. Sci. Eng. 26 (1984) 395.
- [11] S.M.A. Bouwens, R. Prins, V.H.J. de Beer, D.C. Koningsberger, J. Phys. Chem. 94 (1990) 3711.
- [12] S.M.A. Bouwens, J.A.R. Van Veen, D.C. Koningsberger, V.H.J. de Beer, R. Prins, J. Phys. Chem. 95 (1991) 123.
- [13] A.M. van der Kraan, M.W.J. Craje, E. Gerkema, W.L.T.M. Ranselaar, Appl. Catal. 39 (1988) L7.
- [14] M. Breysse, R. Frety, B. Benaichouba, P. Bussiere, Radiochem. Radioanal. Lett. 59 (1983) 265.
- [15] M. Vrinat, M. Breysse, R. Frety, Appl. Catal. 12 (1984) 151.
- [16] M. Breysse, R. Frety, M. Vrinat, Appl. Catal. 12 (1984) 165.
- [17] B. Delmon, in: T. Inui, K. Fujimoto, T. Uchijima, M. Masai (Eds.), New Aspects of Spillover Effect in Catalysis, Elsevier, Amsterdam, 1993, p. 1.
- [18] S. Kasahara, N. Koizumi, J. Iwahashi, M. Yamada, Sekiyu Gakkaishi 38 (1995) 345.
- [19] S. Kasahara, N. Koizumi, M. Yamada, Y. Udagawa, Sekiyu Gakkaishi 38 (1995) 439.